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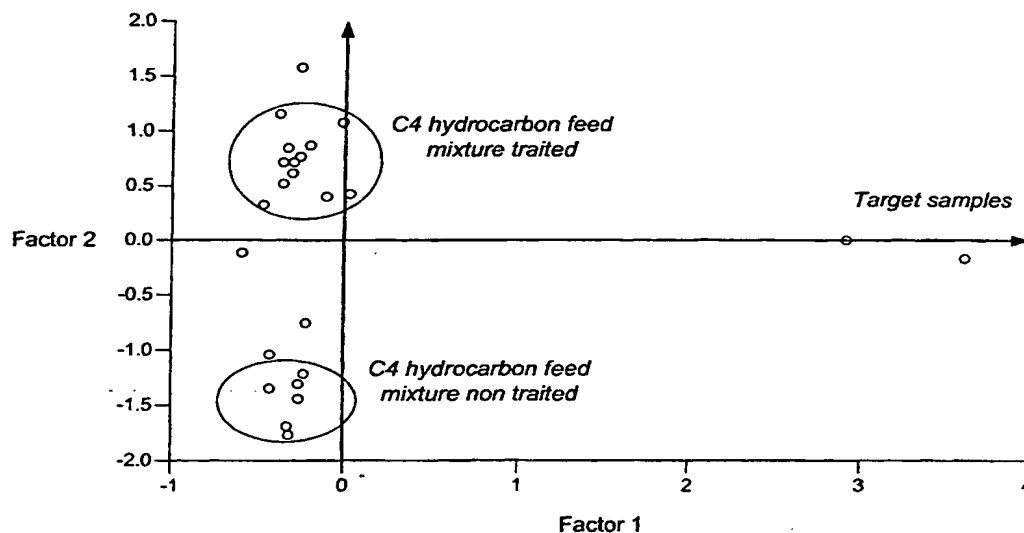
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(54) Title: PROCESS AND APPARATUS FOR POLYMERISATION CATALYST DEVELOPMENT



(57) Abstract: Process for selecting at least one combination among the possible combinations from a group of polymerization catalysts and from a group of sets of polymerization conditions according to the targeted values of one or more properties P_i of the resulting polymers, which process is characterized in that, for each combination, each polymer is subjected to analysis by gas chromatographic pyrolysis and, from the results of the analysis, at least one property P_i of the polymer is evaluated by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and the results of the analysis of the said polymer by gas chromatographic pyrolysis and, in that the combination or combinations corresponding to the desired value of the property or properties P_i is/are selected.

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PROCESS AND APPARATUS FOR POLYMERISATION CATALYST DEVELOPMENT

The field of the present invention is research and development, in particular the development of polymerization catalysts. More specifically, it extends from the synthesis of the polymerization catalysts to the analysis of the polymers, passing through their manufacture from the said catalysts.

5 The present invention relates to a process and to a device for developing polymerization catalysts by directly evaluating the properties of the polymers manufactured from the said catalysts. The present invention makes it possible to rapidly explore a large number of development routes by a systematic approach to the synthesis of the said catalysts, to their uses in the manufacture of polymers and to the method of
10 analysis of the said polymers.

The development of polymerization catalysts is a laborious process which consists in synthesizing a large number of potentially catalytic components and in subsequently selecting according to the catalytic activity.

15 This process, which has been used for a long time, has resulted in the creation of a large number of polymerization catalysts. Also, the advancement in and the miniaturization of robotic techniques make it possible to automate the synthesis of catalysts in order to treat a greater number of samples in a minimum time. New tools are therefore employed in order to allow the development of novel catalysts in a more efficient, economic and systematic way.

20 Patent Application WO 98/03521 discloses a combinatorial synthesis method for the selection and characterization of a group of polymerization catalysts, the said selection being carried out according to characteristics specific to the catalysts. Although this method exhibits obvious improvements in terms of efficiency, of

this method exhibits obvious improvements in terms of efficiency, of reproducibility and of speed, it does not, however, make it possible to easily evaluate the properties and the performance of the targeted final polymer.

5 The properties directly measured on a polymerization catalyst only allow a first evaluation of the performance of the catalyst and of the resulting polymer. A catalyst which is only selected according to its intrinsic properties is not necessarily suited to all polymerization conditions. In order to perform a better evaluation of the polymerization catalysts, it is important to take into account the polymerization conditions and to directly measure the properties of the polymer resulting from the polymerization in the
10 presence of the said catalysts.

On the one hand, taking into account the polymerization conditions necessarily involves having to carry out polymerizations from a selection of catalysts. The use of catalysts in laboratory polymerization reactors is very often a lengthy and tedious process.

15 On the other hand, in order to carry out the evaluation of the essential properties of the polymers resulting from the polymerization in the presence of the above mentioned catalysts, it is necessary to resort to a number of analytical means. These means generally only allow a partial characterization and their use is subject to various restrictions. These restrictions may be related to the amount of sample of polymer, to
20 their preparation and to the duration of the analysis.

These restrictions, related, on the one hand, to the use of the catalysts in laboratory reactors and, on the other hand, to the evaluation of the essential properties of the polymers resulting from the polymerization in the presence of the said catalysts, very often result in prohibitory catalytic research costs.

25 It has been found, in the context of the present invention, to combine the combinatorial synthesis technique with a combinatorial polymerization, allowing the use not only of different catalysts but also of different polymerization conditions. Such a process can only be advantageous if it is used in combination with a means of characterization which can, on the one hand, be automated without penalizing the rate of
30 production of the polymer samples treated and, on the other hand, can make possible the calculation of essential properties of the polymer.

The subject-matter of the present invention is a process for selecting at least one

combination among the possible combinations from a group of polymerization catalysts and from a group of sets of polymerization conditions according to the targeted values of one or more properties P_i of the resulting polymers, which process is characterized in that, for each combination, each polymer is subjected to analysis by gas chromatographic
5 pyrolysis and, from the results of the analysis, at least one property P_i of the polymer is evaluated by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and the results of the analysis of the said polymer by gas chromatographic pyrolysis, and in that the combination or combinations corresponding to the desired value of the property or properties P_i is/are selected.

- 10 The process comprises, for example, the following stages :
- i) synthesizing a group of polymerization catalysts,
 - ii) manufacturing a group of polymers by combination from the group of polymerization catalysts and from the group of the sets of polymerization conditions,
 - 15 iii) isolating a portion or all of each polymer,
 - iv) analysing the said polymers by gas chromatographic pyrolysis, comprising: thermal decomposition of the polymers, passing the resulting pyrolysis gases into one or more gas chromatography columns and digital acquisition of the pyrograms,
 - 20 v) evaluating, from the pyrograms, at least one property P_i of the polymer by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and pyrograms of the said polymers, and
 - vi) selecting at least one combination among the combinations prepared from the group of the polymerization catalysts and from the group of the sets of
25 polymerization conditions, by comparison of the properties P_i with their targeted values.

According to the present invention, the term "polymerization catalyst" is understood to mean any catalyst having one or more catalytic components, comprising, for example, a catalyst in combination with a cocatalyst, capable of polymerizing a
30 monomer or copolymerizing a monomer with at least one comonomer. The catalyst can take part in both homogeneous polymerization catalysis and of heterogeneous polymerization catalysis. Thus, the catalyst can be employed in the solid or liquid form or

in solution in the polymerization medium. It can be used as is or supported on a solid, such as a metal oxide or a refractory oxide. It can also be used in the form of a prepolymer, that is to say of a catalyst which has been subjected to a preliminary stage of polymerization of one or more monomers which are identical to or different from that of the subsequent main polymerization.

The catalyst can be a compound which generates free radicals, such as a peroxide, a hydroperoxide or a persalt, in particular an organic version, or an azo compound, for example benzoyl peroxide, dicumyl peroxide, chlorobenzoyl peroxide, tert-butyl perbenzoate, lauroyl peroxide or azobisisobutyronitrile, or sodium or potassium persulphate. Such a catalyst takes part in a radical polymerization, such as, for example, an alkene polymerization, such as ethylene, or a vinyl polymerization, such as a polymerization of vinyl chloride or of an acrylic ester or of acrylonitrile or of an aromatic vinyl compound, for example styrene or α -methylstyrene.

The catalyst can be a cationic catalyst, for example formed by the addition of an acid compound to an alkene. The acid compound can be sulphuric acid, hydrofluoric acid, aluminium chloride or boron trifluoride, in particular a catalyst of Friedel-Crafts type. The alkene can carry an electron-donating group, so that the intermediate cation formed is sufficiently stable to allow the polymerization to progress. Such a catalyst is involved, for example, in the polymerization of isobutene.

The catalyst can also be an anionic catalyst, for example a powerful nucleophilic reagent, which, for example added to an alkene, gives a carbanion. An anionic catalyst can be an organometallic compound, such as n-butyllithium. Such a catalyst is involved, for example, in the polymerization of isoprene.

The catalyst can also be a catalyst of Ziegler-Natta type comprising a catalyst proper, based on a transition metal, such as a halide of a transition metal, for example a titanium or vanadium or zirconium chloride, in combination with a cocatalyst, such as an organometallic compound, for example an organoaluminium.

The catalyst can be in particular a metallocene, especially of a transition metal, such as zirconium, hafnium, titanium or chromium.

The catalyst can also be a chromium oxide compound supported on a refractory oxide which is thermally activated, such as a catalyst of Phillips type. Such a catalyst is involved in the olefin polymerization, such as ethylene or propylene or a butene.

According to the present invention, each component of the group of the polymerization catalysts can be distinguished by its method of synthesis. By way of example, the methods of synthesis can be distinguished by the nature, the amount and the flow rates of the reactants or additives. They can also be distinguished, for example, by the physical parameters of the synthesis, such as the temperature or the pressure. This results in polymerization catalysts which can differ in their compositions, their types (homogeneous or heterogeneous), their forms (solid, liquid, in solution in the polymerization medium, and the like) and their physical, chemical or physicochemical properties. The said catalysts can optionally also differ, inter alia, in the nature and the concentration of the cocatalyst used, the type of support, the type of coating, the presence or absence of a prepolymerization and the degree of progression and the nature of the (co)monomers of the said prepolymerization and the method of activation.

According to the present invention, a group of polymerization catalysts is synthesized. This operation can be carried out by any known laboratory or industrial method. This operation is preferably carried out by combinatorial synthesis methods which make it possible to rapidly manufacture a large number of catalysts by virtue of appropriate automation and miniaturization of the equipment used.

According to the present invention, it is possible to characterize the catalysts obtained by synthesis. This characterization can be carried out by methods chosen from gas chromatography, differential calorimetry, scanning thermal microscopy or any rheological method.

According to the present invention, the term "sets of polymerization conditions" is understood to mean categories of conditions necessary for carrying out a polymerization. The reaction medium, the method of stirring, the reactants, the additives and all the physical quantities which can be controlled within the polymerization reactor can be chosen, for example, in order to constitute a set of polymerization conditions.

The reaction medium can be a liquid phase comprising hydrocarbons, for example a solvent, or else a liquid phase composed of the monomer or the manufactured polymer in the molten state. The reaction medium can also be a gas comprising, for example, the (co)monomers and inert gases. The inert gases can be alkanes, such as pentane, nitrogen or a mixture of nitrogen and alkanes. The method of stirring can be chosen from any known stirring technique. It can be, for example, internal stirring by a mechanical stirrer

or external stirring, such as by movement or vibration of the reactors or of the solid structure supporting them, for example ultrasound vibration. It can also be stirring by bubbling or fluidization. The polymerization reactants can be monomers, comonomers or chemical chain-termination compounds. The additives can be any compound which has
5 an impact on the properties of the polymer when it is added during the polymerization, such as chemical activators or crosslinking agents. The physical quantities which can be controlled within the polymerization reactor can be the temperature, the pressure, the concentrations, the composition and the flow rates of the compounds of the reaction medium.

10 According to the present invention, a group of polymers is manufactured by combination from the group of polymerization catalysts and from the group of the sets of polymerization conditions. The term "combination" is understood to mean bringing a polymerization catalyst into contact with at least one monomer while using a set of polymerization conditions. This operation is preferably carried out by methods which
15 make it possible to rapidly manufacture a large number of polymers by virtue of appropriate automation and miniaturization of the equipment used. The group of catalysts is preferably obtained from a combinatorial synthesis method, which makes it possible to have an automated process comprising, on the one hand, the synthesis of the catalysts and, on the other hand, the manufacture of the polymers.

20 The number of polymers manufactured can be between unity and the number of the combinations possible from the group of polymerization catalysts and from the group of the sets of polymerization conditions. For example, if the group of polymerization catalysts comprises N separate catalysts and the group of the sets of polymerization conditions comprises M sets, it is possible to carry out $N \times M$ combinations, resulting in
25 $N \times M$ presumed distinct polymers.

According to a specific case of the present invention, it is possible to combine a single catalyst with a group of sets of polymerization conditions. In the same way, it is possible, according to another specific case of the present invention, to combine a group of catalysts with a single set of polymerization conditions. These two specific cases can
30 constitute preferred forms of the present invention.

The amount of each polymer manufactured can be between 1 mg and 100 g, preferably from 100 mg to 10 g. An excessively large amount of polymer is penalizing in

terms of use of the process of the invention, in particular of use of automated equipment allowing rapid treatment of a large number of samples.

5 A preferred condition of the present invention is the miniaturization of the samples of catalyst and of polymer, in order to rapidly treat a large number of polymers in a minimum time. In order to meet this condition of miniaturization, the manufacture of the polymers can be carried out in microreactors, within which a polymerization catalyst is combined with a set of polymerization conditions by combination from the group of polymerization catalysts with the group of the sets of polymerization conditions.

10 The microreactors can be chosen according to the sets of polymerization conditions applied. The possibilities are unlimited but, for obvious reasons of practicality, it is preferable to use identical microreactors. Use may be made, among the types of microreactor, of, for example, tubular glass microreactors equipped with injection devices within which the catalysts are immersed in a solvent. The monomer and optionally the comonomer or comonomers can be injected simultaneously by bubbling
15 into the microreactors using injectors mounted on an appropriate structure. The microreactors can be stirred by mechanical vibrations of the combined structure supporting the microreactors.

The microreactors used should generally meet the conditions imposed by the different polymerizations, such as, for example, the purity of the reactants, the stirring,
20 the pressure and the temperature.

A preferred condition of the present invention is the automation of the process for the manufacture of the polymers. The group of the sets of polymerization conditions is preferably suitable for the process to be automated. It is preferable to choose, for example, a reaction medium which is simple to employ, such as a solvent, in comparison
25 with a gas. Likewise, it is preferable to choose, for example, a method of stirring by vibration of the structure supporting the microreactors, in comparison with a fluidized bed.

Another preferred condition of the present invention is the speed of execution during the manufacture of the polymers. Miniaturization and automation can make it
30 possible to meet this condition. The time for manufacture of the polymers can be between 10 seconds and 15 minutes, preferably between 20 seconds and 10 minutes.

According to the present invention, it is possible to isolate a portion or all of each

polymer. In particular, it is possible to withdraw samples of each polymer. This withdrawing can be carried out by any appropriate technical means. The weight of the samples must be sufficient to allow analysis by gas chromatographic pyrolysis. This withdrawing can be carried out, for example, under an atmosphere purified by an inert gas, such as nitrogen or argon.

By way of example, the polymer samples can be withdrawn by deposition on a component which can be, for example, a ferromagnetic component, the said ferromagnetic component also having an essential function described subsequently in the description of the analysis by gas chromatographic pyrolysis. It is possible, in this case, to use a movable structure to which the said components are attached. To carry out the sampling, the said components are immersed in the polymerization microreactors. A fine polymer film, which in the case of this example is in the form of a gel, is deposited on the said components. The latter can subsequently be collected and introduced individually into a pyrolysis chamber by any mechanism, which mechanism is preferably automated, such as a turntable.

According to another form of the present invention, all of each polymer is isolated in the polymerization microreactor where it was manufactured and is transferred into a pyrolysis chamber.

According to yet another form of the present invention, the microreactor is also the pyrolysis chamber.

According to the present invention, the polymer samples are analysed by gas chromatographic pyrolysis.

Analysis by gas chromatographic pyrolysis generally comprises at least one stage of thermal decomposition during which the polymer samples are brought to a temperature which is sufficient to bring about decomposition by cleavage of the molecular chains. This temperature, subsequently known as the pyrolysis temperature, can vary according to the type of polymer analysed. The polymer samples can be subjected to heat treatment during which the temperature varies, with at least one passage above the pyrolysis temperature. According to a preferred form of the present invention, preheating at a temperature below the pyrolysis temperature, that is to say which does not bring about thermal decomposition, can be carried out in order to remove the liquid or gaseous compounds existing in the said samples which might

influence the results of the analysis by gas chromatographic pyrolysis. According to another preferred form of the present invention, a temperature beyond the pyrolysis temperature can be applied to the polymer samples with a virtually instantaneous rise in the temperature. The thermal decomposition operation is preferably carried out in a non oxidizing atmosphere, preferably an inert atmosphere, so as to avoid any combustion.

The analysis by gas chromatographic pyrolysis generally also comprises passing the pyrolysis gases into one or more gas chromatography columns. The gas chromatography columns can be different in length and can operate with different flow rates of carrier gases, in order to optimize the compromise between the duration of the analysis and the resolution of the pyrograms. The columns can also be different in nature, such as packed columns or capillary columns with an appropriate stationary phase. The detector of the chromatograph can be adjusted to the nature of the pyrolysis gases. It is possible, for example, to use a mass spectrometer, separately or coupled with gas chromatography. It is possible to use other types of detectors, such as flame ionization detectors (FID) or thermal conductivity cells.

Any technology targeted at reducing the duration of analysis can be employed, such as the "back flush" technique or high pressure fast gas chromatography or GC. It is also possible to employ a hydrogenation stage which makes it possible to simplify the analysis of the pyrograms obtained.

The analysis by gas chromatographic pyrolysis can optionally comprise digital acquisition of the pyrograms. This is preferably carried out with a computer. The said acquisition can make it possible to display the pyrograms for each polymer sample, to carry out digital processing resulting in the interpretation of the said pyrograms and in particular to carry out the selection according to the process of the present invention.

According to the present invention, at least one property P_i of the polymer is evaluated from the pyrograms by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and pyrograms. A pyrogram can be described as a function of a retention time in a chromatographic column of the constituents of the pyrolysis gases, the amplitude or the surface of which is a function of the amount of the said compounds. A pyrogram is often provided as a curve comprising a succession of peaks, the main parameters of which are principally the distance between each peak and a temporal reference point and the area of the said peaks. From these parameters, it is

possible to differentiate the constituents of the pyrolysis gases by their molecular weights and to determine their respective amounts. To identify the constituents of the pyrolysis gases, each pyrogram can be compared with a library of pyrograms corresponding to known compounds which were analysed by conventional analytical means. This method
5 can be employed by a computer in parallel with the digital acquisition of the pyrograms.

It is possible, by analysis by gas chromatographic pyrolysis, to characterize the polymer samples according to their mechanisms of thermal decomposition. By way of example, the polymer samples can be characterized by intramolecular properties, such as the nature and the amount of comonomer and the number, the length and the distribution
10 of the branchings. This makes it possible, for example, to carry out selections by polyethylene classes.

The approach described in this example can be generalized to quantify one or more properties P_i . This evaluation from the pyrograms of at least one property P_i of the polymer can comprise the following stages:

- 15 i) as described above, a prior digital processing in order to identify the constituents of the pyrolysis gases on the pyrograms, by virtue of a library of pyrograms corresponding to known compounds,
- ii) as described above, a calculation of the main parameters of the pyrograms, and
- iii) the calculation of the properties P_i by virtue of correlations drawn up beforehand
20 between the property or properties P_i of the polymers and the main parameters of the pyrograms. The correlations are drawn up from a databank linking the properties of the polymers and their pyrograms, the said properties having been measured by conventional analytical methods. By virtue of these correlations, it is possible to determine a large number of properties P_i and in particular the
25 properties related to the intramolecular structure of the polymers which generally influence the intermolecular properties.

According to the present invention, a selection is made of at least one combination among the combinations prepared from the group of polymerization catalysts and from the group of the sets of polymerization conditions, by comparison of
30 the calculated properties P_i with their targeted values.

According to the present invention, the properties P_i of the polymer, from which properties the selection is made, are accessible by a gas chromatographic pyrolysis

technique. The term "accessible properties" is understood to mean any property P_i which can be determined from a pyrogram such as those that have been described above.

The properties P_i can be chosen from the intra- or intermolecular structural properties and/or the physical properties. The intra- or intermolecular structural
5 properties can be the molecular mass, the distribution of the molecular masses, the nature and the length of the branchings, the distribution of the branchings, the tacticity, the concentration of comonomer(s) and the crystallinity. The physical properties can be the mechanical, optical, rheological, kinetic or flow properties.

The present invention also relates to equipment which allows the process of the
10 invention to be implemented and which comprises the following components:

- optionally a device for the combinatorial synthesis of polymerization catalysts,
- a group of polymerization microreactors and optionally a device for feeding the said microreactors with polymerization catalysts,
- a device for injecting the (co)monomer or (co)monomers and optionally reactants and
15 additives into the said microreactors,
- a device for placing under polymerization conditions,
- one or more pyrolysis chambers comprising at least one heating system, at least one pipe for feeding with inert gas and at least one pipe for discharging the inert and pyrolysis gases, at least one of the said discharge pipes being connected to one or
20 more columns of a gas chromatography device,
- optionally a device for isolating the polymer produced in the microreactors and for transferring the isolated part into the pyrolysis chamber or chambers, and
- a computer connected to at least one gas chromatography device.

According to a preferred form, the equipment of the present invention comprises
25 a device for the combinatorial synthesis of polymerization catalysts. This device can be decoupled from the equipment, which involves the manual transfer of the polymerization catalysts into the microreactors. This device can also be coupled to the equipment according to the invention via an automaton, making it possible to carry out automated transfer of the polymerization catalysts into the microreactors. This device can also form
30 an integral part of the equipment according to the invention, using, for example for the synthesis of polymerization catalysts, the same microreactors subsequently used for the polymerization in the presence of the said catalysts.

According to the present invention, the equipment comprises a group of microreactors. The latter can be, as described above, adjusted to the sets of polymerization conditions and to the catalysts used.

5 The equipment of the present invention can comprise a device for injecting the (co)monomer(s) and optionally reactants and additives into the said microreactors. By way of example, this device can be a robot arm, at the end of which are mounted injection syringes delivering controlled doses of (co)monomer(s), of reactants and of additives. In the case of this example, the microreactors can be equipped with leaktight membrane(s), allowing injection under purity conditions suited to the process of the
10 present invention.

The equipment of the present invention can comprise a device for placing under polymerization conditions. This device can comprise, for example, a heating and cooling system, a stirring system, a pressurization system and any system allowing use of the sets of polymerization conditions.

15 The equipment of the present invention can comprise one or more pyrolysis chambers. A pyrolysis chamber can comprise at least one heating system. According to a preferred form of the present invention, the heating system can be a ferromagnetic component which, by high frequency electromagnetic induction, can rise virtually instantaneously to the temperature of the Curie point of the component. The heating
20 temperature is generally a function of the composition of the alloy of the ferromagnetic component. The heating system can comprise an additional heating device for temperatures below the pyrolysis temperature. A pyrolysis chamber can also comprise at least one pipe for feeding with inert gas. The latter can be connected to a store of inert gas and can be equipped with a device allowing the flow rate of the said gas to be
25 controlled. A pyrolysis chamber can also comprise at least one pipe for discharging the inert and pyrolysis gases. At least one of the said discharge pipes can be connected to one or more columns of a gas chromatography device.

Use may be made of an equipment for analysis by Joule-effect pyrolysis which makes possible gradual heating of the sample by temperature increment. Among the
30 equipment of this type, it is possible to choose those sold by CDS Analytical Inc. (USA) under the name "CDS Pyroprobes"^(®), Models "1000"^(®) and "2000"^(®). Use is preferably made of an equipment for analysis by Curie-point pyrolysis which makes possible perfect

reproducibility and a virtually instantaneous rise in the pyrolysis temperature. Among the equipments of this type, it is possible to choose the one sold by Fischer (Germany) under the trade name Fischer-CSG^(®).

5 In a specific case of the present invention, each microreactor can be used as pyrolysis chamber.

The equipment of the present invention can optionally comprise a device for isolating the polymer produced in the microreactors and for transferring the isolated part into the pyrolysis chamber or chambers. According to a preferred form, the said device can be a device for sampling a polymer. By way of example, use may be made of one or
10 more ferromagnetic components as described above which simultaneously act as heating system for the pyrolysis chamber or chambers. A first advantage of the present invention is the speed of the perfecting of novel catalysts by an approach which makes it possible, in a minimum time, to test a large number of combinations of polymerization catalysts and of sets of polymerization conditions and to rapidly know, by virtue of the analysis by
15 gas chromatographic pyrolysis, the properties of the polymer thus produced with a very small amount of sample.

A second advantage lies in the fact that the evaluation of the catalysts performance is carried out directly from the polymer resulting from the combinations of polymerization catalysts and of sets of polymerization conditions.

20 A third advantage is related to the automation of the process, allowing very good reproducibility of the results.

A fourth advantage is related to the miniaturization of the process, allowing the properties of the resulting polymer to be evaluated on small-sized samples.

A fifth advantage lies in reducing the research costs in the development and the
25 perfecting of the catalysts.

A sixth advantage lies in the systematic approach of the process which makes it possible to more fully cover the various arrangements possible in the combinations of polymerization catalysts and of sets of polymerization conditions.

A seventh advantage, resulting from the preceding advantage, lies in the
30 limitation of the risks taken in extrapolating to an industrial scale.

An eighth advantage lies in the principle of the analysis by gas chromatographic pyrolysis of the process, making it possible, by appropriate modelling, to anticipate the

behaviour of the polymer during its conversion to finished items, this being achieved directly during the development and the perfecting of the catalysts.

Example 1

Impact of the organometallic content in polymerization catalyst and the
5 polymerization temperature on the structural properties of the resulting polyethylene.

The present example was carried out in order to select combinations, from a group of polymerization catalysts having different concentration of tri-n-octylaluminium compound (or TnOA) and from a group of polymerization temperatures, said combinations conferring to the resulting polyethylene differentiated structural properties.

10 The polymerization catalysts used were of the Ziegler-Natta type based on titanium, supported on magnesium chloride and comprising tri-n-octylaluminium (or TnOA). The group of polymerization catalysts had, in the present example, three different catalysts, each of them having a different molar ratio of the aluminium over the titanium compounds, Al/Ti, of 0.8, 1.2 and 1.5, all the other characteristics being
15 maintained identical.

The polymerization reactions using those catalyst were carried out in identical gas phase reactors, said gas phase comprising by weight 30 % of ethylene, 10 % of hydrogen, 10 % of 1-butene and 50 % of nitrogen by weight. The absolute pressure maintained in the reactors was 0.5 MPa. The butene and hydrogen partial pressure were
20 maintained constant during the whole polymerization. The group of sets of polymerization conditions had four different sets, each of them having a different polymerisation temperature of 65°C, 75°C, 80°C and 90°C, all the other polymerization conditions being maintained identical.

The combinations from the group of three polymerization catalysts having a
25 different TnOA content and from the group of four sets of polymerization conditions having different polymerization temperature resulted in the manufacturing of twelve polyethylene samples that were subjected to an analysis by gas chromatographic pyrolysis under the same conditions, in accordance with the present invention.

The gas chromatographic pyrolysis was carried out using a Curie-point micro-
30 pyrolyser sold by Fischer under the trade name Fischer-CSG®. Each sample was preheated at a temperature of 250°C and submitted to a pyrolysis temperature of 670°C for 15 seconds. The pyrolysis gases were passed into a fused-silica capillary column

coated with a film of 0.25 μm of chemically bonded cross linked methylsilicone sold by RESTEK under the name of RTX1®, having a length of 30 m, an internal diameter of 0.25 m using nitrogen as a carrier gas. The gas chromatographic apparatus used was sold by CHROMPACK under the name CHROMPACK-CP-9001® and was equipped with a
5 flame ionization detectors (FID) .

The gas chromatographic pyrolysis analysis led to twelve different pyrograms corresponding to the twelve polyethylene samples above mentioned.

The objective was to select combinations of polymerization catalyst and polymerization temperature conferring differentiated properties to the resulting
10 polyethylene. The properties that were taken into account in the present example were: P1: the concentration of isolated butene unit in the macromolecular chain, and P2: the concentration by weight of butene.

By virtue of correlations drawn up beforehand between, the properties P1 and P2, and the results of the pyrolysis gas chromatographic analysis, it has been possible to
15 evaluate P1 and P2, for the twelve polyethylene samples from the results of pyrolysis gas chromatographic analysis.

The correlations between P1 and P2, and the results of the pyrolysis gas chromatographic analysis were expressed as a function of the pyrogram peak surfaces, S_i , having specific retention time, i and j . The correlations that were expressed as
20 following:

$$P1 = \sum_i A_i * S_i^{B_i}$$
$$P2 = \sum_j A_j * S_j^{B_j}$$

where A_i , B_i , A_j , and B_j are constants.

The properties P1 and P2 obtained for the twelve polyethylene samples are presented in Tables 1, 2 and 3 corresponding to an Al/Ti molar ratio in the catalyst
25 respectively of 0.8, 1.2 and 1.5.

Table 1

Polymerization Temperature (°C)	65	75	80	90
Al/Ti=0.8				
P1 (%)	92.3	84.7	82.4	85.0
P2 (%)	5.8	5.7	7.8	7.3

Table 2

5

Polymerization Temperature (°C)	65	75	80	90
Al/Ti=1.2				
P1 (%)	87.0	88.3	88.0	86.0
P2 (%)	6.8	8.2	8.3	8.0

Table 3

Polymerization Temperature (°C)	65	75	80	90
Al/Ti=1.5				
P1 (%)	88.0	83.0	80.1	81.2
P2 (%)	6.2	7.8	7.6	7.6

10 From the above tables, a selection was made of the combinations between the polymerization catalyst and polymerization temperature conferring the best compromise between a high concentration of isolated butene unit in the macromolecular chain (P1) and a high concentration by weight of butene (P2). It was found that using a polymerization catalyst having a ratio Al/Ti equal to 1.2 at a polymerization temperature

15 of 75°C or 80°C allows to manufacture a polyethylene having the best compromise in term of structural properties, offering in the same time smooth operating conditions, particularly in terms of polymerization temperature.

Example 2

20 Impact of the C4 hydrocarbon feed mixture composition used to manufacture polyisobutene on the structural properties of the said polyisobutene, more particularly on

its unsaturated terminations distribution and more specifically on its reactivity.

The present example was achieved to identify the effect of an hydrogenation treatment of the C4 hydrocarbon feed mixture on the polyisobutene reactivity.

5 The concept of reactivity of a polyisobutene used in this example aims to reflect the reaction yield and the selectivity of the polyisobutene during post chemical treatment (for instance, maleisation) . This concept of reactivity was not properly quantified and its evaluation was made by comparison of the unsaturated terminations distribution in the polyisobutene. From experience, it was known that the unsaturated terminations distribution in a polyisobutene was somehow correlated to the surface of pyrogram
10 peaks having specific retention times.

The present example is based on a statistical analysis, and more particularly a factor analysis, on data from a population of polyisobutene samples analysed by pyrolysis gas chromatography, said samples having been produced using the same catalyst and different C4 hydrocarbon feed mixture. Two polyisobutene products known for their
15 good reactivity, referred as target sample, were included into the polyisobutene samples population after having been submitted to the same pyrolysis gas chromatography.

The catalyst system used in the present example was an ethyldichloroaluminium. The weight ratio between the catalyst and the cocatalyst was initially equal to 1.25.

20 The polymerization reactions were carried out in a boiling liquid reaction phase containing the isobutene from the C4 hydrocarbon feed, the polymer being formed and the catalyst system. The polymerization reactions were carried out at a temperature of 10°C and at an absolute pressure of 0.132 MPa. The only parameter that was varied between was the quality of the C4 hydrocarbon feed mixture, and more specifically whether the C4 hydrocarbon was submit or not to an hydrogenation treatment. Two sub-
25 populations of polyisobutene were manufactured one with hydrogenation treatment, and the other one without any treatment, of the C4 hydrocarbon feed mixture prior to the polymerization reactions.

The objective of a factor analysis is to determine how each variable of a given set of variables are related to each other. The set of variables chosen for the present example
30 were the concentrations of n-butene, trans-2-butene, cis-2-butene, 1-butene in the C4 hydrocarbon feed mixture and the surfaces of six different peaks of the resulting pyrograms, each of said peaks having a specific retention time. From the factor analysis

it was possible to position the polyisobutene and target samples in a co-ordinate axis system wherein each axis corresponds to one of the factors of the factor analysis as plotted in Figure 1.

From this plot, the sub-population of polyisobutene obtained from a non treated C4 hydrocarbon feed mixture, the sub-population of polyisobutene obtained from a treated C4 hydrocarbon feed mixture and the two target samples were clearly distinctively separated. It appears that both populations A and B are equally far from the target samples which means that no improvement, in terms of reactivity, has to be expected by achieving the hydrogenation treatment of the C4 hydrocarbon feed mixture under these operating conditions.

This conclusion could have been drawn from a very long and costly RMN analysis of the polyethylene samples. This example illustrates the rapidity and flexibility of the process of the present invention.

Claims:

1. Process for selecting at least one combination among the possible combinations from a group of polymerization catalysts and from a group of sets of polymerization conditions according to the targeted values of one or more properties P_i of the resulting polymers, which process is characterized in that, for each combination, each polymer is
5 subjected to analysis by gas chromatographic pyrolysis and, from the results of the analysis, at least one property P_i of the polymer is evaluated by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and the results of the analysis of the said polymer by gas chromatographic pyrolysis and, in that the combination or combinations corresponding to the desired value of the property or
10 properties P_i is/are selected.
2. Process according to Claim 1, characterized in that it comprises the following stages:
 - i) synthesizing a group of polymerization catalysts,
 - ii) manufacturing a group of polymers by combination from the group of
15 polymerization catalysts and from the group of the sets of polymerization conditions,
 - iii) isolating a portion or all of each polymer,
 - iv) analysing the said polymers by gas chromatographic pyrolysis, comprising:
20 thermal decomposition of the polymers, passing the resulting pyrolysis gases into one or more gas chromatography columns and digital acquisition of the pyrograms,
 - v) evaluating, from the pyrograms, at least one property P_i of the polymer by virtue

of correlations drawn up beforehand between the property or properties P_i of the polymers and pyrograms of the said polymers, and

- vi) selecting at least one combination among the combinations prepared from the group of the polymerization catalysts and from the group of the sets of polymerization conditions, by comparison of the properties P_i with their targeted values.

3. Process according to Claim 1 or 2, characterized in that a single catalyst is combined with a group of sets of polymerization conditions.

4. Process according to Claim 1 or 2, characterized in that a group of catalysts is combined with a single set of polymerization conditions.

5. Process according to any one of Claims 1 to 4, characterized in that the amount of each polymer resulting from the combination can be between 1 mg and 100 g, preferably from 100 mg to 10 g.

6. Equipment comprising the following components:

- a group of polymerization microreactors and optionally a device for feeding the said microreactors with polymerization catalysts,
- a device for injecting the (co)monomer or (co)monomers and optionally reactants and additives into the said microreactors,
- a device for placing under polymerization conditions,
- one or more pyrolysis chambers comprising at least one heating system, at least one pipe for feeding with inert gas and at least one pipe for discharging the inert and pyrolysis gases, at least one of the said discharge pipes being connected to one or more columns of a gas chromatography device, and
- a computer connected to at least one gas chromatography device.

7. Equipment according to Claim 6, characterized in that it comprises a device for the combinatorial synthesis of polymerization catalysts.

8. Equipment according to anyone of Claims 6 and 7, characterized in that it comprises a device for isolating the polymer produced in the microreactors and for transferring the isolated part into the pyrolysis chamber or chambers.

9. Equipment according to any one of Claims 6 to 8, characterized in that the pyrolysis chamber(s) is (are) apparatus(es) for Curie-point pyrolysis.

AMENDED CLAIMS

[received by the International Bureau on 04 January 2001 (04.01.01);
original claims 1-9 replaced by new claims 1-11 (3 pages)]

- 5 1. Process for selecting at least one combination
among the possible combinations from a group of
polymerization catalysts and from a group of sets of
polymerization conditions according to the targeted
values of one or more properties P_i of the resulting
10 polymers, which process is characterized in that, for
each combination, each polymer is subjected to analysis
by gas chromatographic pyrolysis and, from the results
of the analysis, at least one property P_i of the
polymer is evaluated by virtue of correlations drawn up
15 beforehand between the property or properties P_i of the
polymers and the results of the analysis of the said
polymer by gas chromatographic pyrolysis and, in that
the combination or combinations corresponding to the
desired value of the property or properties P_i is/are
20 selected.
2. Process according to Claim 1 characterized in that
the property P_i of the polymers is chosen from the
intra-molecular structural properties and/or the
physical properties.
- 25 3. Process according to Claim 1 characterized in that
the property P_i of the polymers is chosen from the
physical properties.
4. Process according to any one of Claims 1 to 3,
characterized in that it comprises the following
30 stages:
- i) synthesizing a group of polymerization catalysts,
 - ii) manufacturing a group of polymers by combination
from the group of polymerization catalysts and
from the group of the sets of polymerization
35 conditions,
 - iii) isolating a portion or all of each polymer,
 - iv) analysing the said polymers by gas chromatographic
pyrolysis, comprising: thermal decomposition of
the polymers, passing the resulting pyrolysis

- gases into one or more gas chromatography columns and digital acquisition of the pyrograms,
- v) evaluating, from the pyrograms, at least one property P_i of the polymer by virtue of correlations drawn up beforehand between the property or properties P_i of the polymers and pyrograms of the said polymers, and
- vi) selecting at least one combination among the combinations prepared from the group of the polymerization catalysts and from the group of the sets of polymerization conditions, by comparison of the properties P_i with their targeted values.
5. Process according to any one of Claims 1 to 4, characterized in that a single catalyst is combined with a group of sets of polymerization conditions.
6. Process according to any one of Claims 1 to 4, characterized in that a group of catalysts is combined with a single set of polymerization conditions.
7. Process according to any one of Claims 1 to 6, characterized in that the amount of each polymer resulting from the combination can be between 1 mg and 100 g, preferably from 100 mg to 10 g.
8. Equipment comprising the following components:
- a group of polymerization microreactors and optionally a device for feeding the said microreactors with polymerization catalysts,
 - a device for injecting the (co)monomer or (co)monomers and optionally reactants and additives into the said microreactors,
 - a device for placing under polymerization conditions, one or more pyrolysis chambers comprising at least one heating system, at least one pipe for feeding with inert gas and at least one pipe for discharging the inert and pyrolysis gases, at least one of the said discharge pipes being connected to one or more columns of a gas chromatography device, and
 - a computer connected to at least one gas chromatography device.

9. Equipment according to Claim 8, characterized in that it comprises a device for the combinatorial synthesis of polymerization catalysts.
10. Equipment according to anyone of Claims 8 and 5 9, characterized in that it comprises a device for isolating the polymer produced in the microreactors and for transferring the isolated part into the pyrolysis chamber or chambers.
11. Equipment according to any one of Claims 8 to 10 10, characterized in that the pyrolysis chamber(s) is (are) apparatus(es) for Curie-point pyrolysis.

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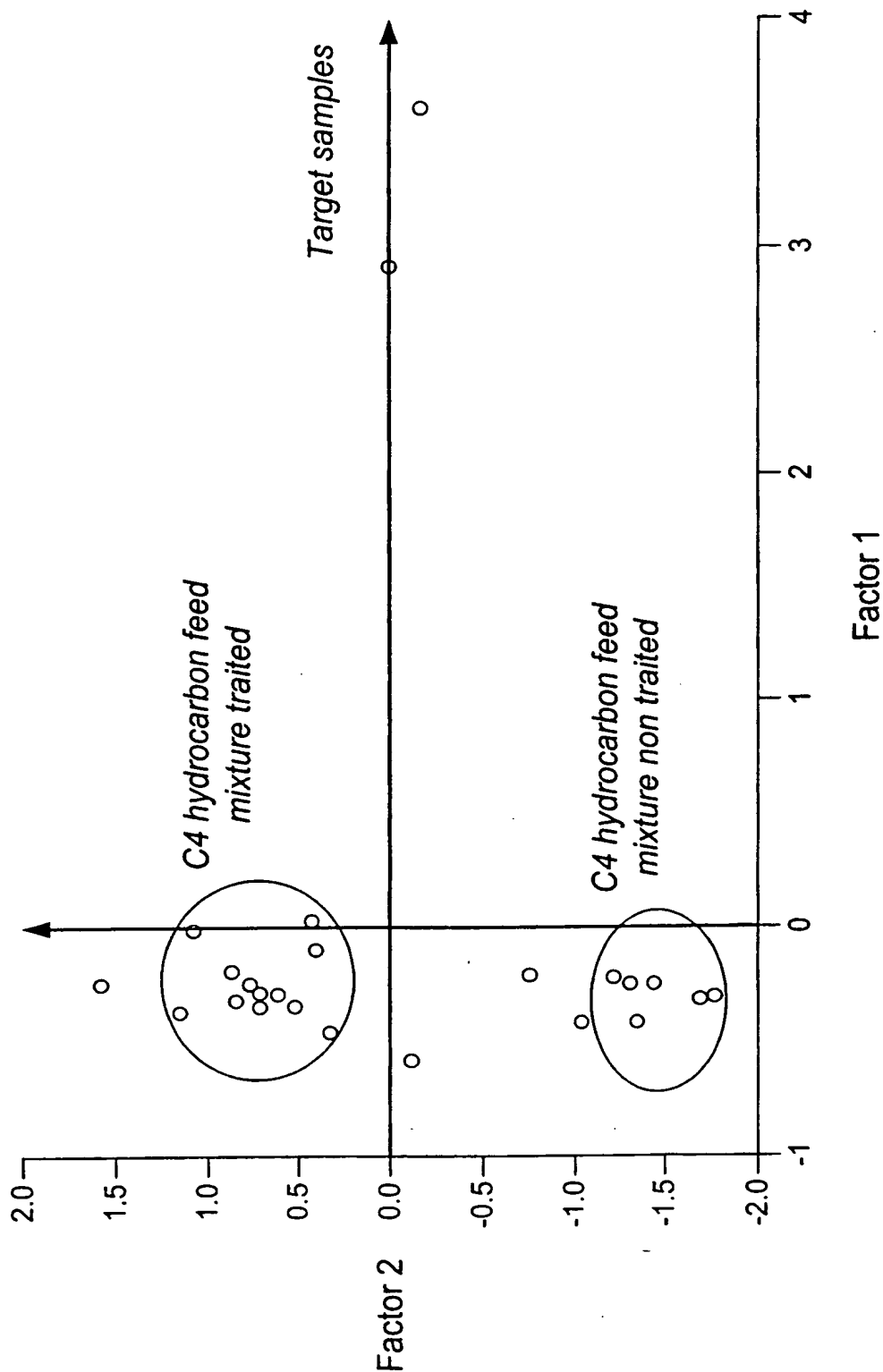


Fig. 1

INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 00/03532

A. CLASSIFICATION OF SUBJECT MATTER

IPC 7 C07B61/00 B01J19/00 C08F2/00 G01N35/00

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC 7 B01J C07B G01N C08F

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

Electronic data base consulted during the international search (name of data base and, where practical, search terms used)

EPO-Internal, WPI Data, PAJ, INSPEC, COMPENDEX

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	DUC S ET AL: "Investigations of the thermodegradation of ethylene-alpha-olefin copolymers by pyrolysis-gas chromatography (Py-GC)", POLYMER, GB, ELSEVIER SCIENCE PUBLISHERS B.V, VOL. 40, NR. 24, PAGE(S) 6723-6728 XP004177307	1-5
A	ISSN: 0032-3861 The entire doct.	6-9
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Further documents are listed in the continuation of box C.



Patent family members are listed in annex.

* Special categories of cited documents :

"A" document defining the general state of the art which is not considered to be of particular relevance

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Date of the actual completion of the international search

31 October 2000

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16/11/2000

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INTERNATIONAL SEARCH REPORT

International Application No

PCT/GB 00/03532

C.(Continuation) DOCUMENTS CONSIDERED TO BE RELEVANT

Category *	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
A	<p>DATABASE COMPENDEX 'Online! ENGINEERING INFORMATION, INC., NEW YORK, NY, US; OHTANI HAJIME ET AL: "Pyrolysis-gas chromatographic study of end groups in poly(methyl methacrylate) radically polymerized in toluene solution with benzoyl peroxide as initiator" Database accession no. EIX89070915829 XP002151563 abstract & PROCEEDINGS OF THE 8TH INTERNATIONAL SYMPOSIUM ON ANALYTICAL AND APPLIED PYROLYSIS; LUND, SWITZ JUN 13-17 1988, vol. 15, 13 June 1988 (1988-06-13), pages 167-174, J Anal Appl Pyrolysis Mar 1989</p>	1-9
A	<p>PETIT A ET AL: "POLYMERISATION RADICALEAIRE DU PENTADIENE-1,3. \IV. DETERMINATION DE LA COMPOSITION ET DU RUN NUMBER DES COPOLYMERES DE CIS- OU TRANS-PENTADIENE-1,3 ET D'ACRYLONITRILE PAR PYROLYSE ECLAIR COUPLEE A LA CHROMATOGRAPHIE EN PHASE GAZEUSE*", JOURNAL OF APPLIED POLYMER SCIENCE, US, JOHN WILEY AND SONS INC. NEW YORK, VOL. 41, NR. 1 / 02, PAGE(S) 267-299 XP000216579 ISSN: 0021-8995 page 297</p>	1-9
A	<p>VAN DER HAGE E R E ET AL: "On-line Curie-point pyrolysis-high-performance liquid chromatographic-mass spectrometric analysis of lignin polymers", JOURNAL OF CHROMATOGRAPHY A, NL, ELSEVIER SCIENCE, VOL. 736, NR. 1, PAGE(S) 61-75 XP004039045 ISSN: 0021-9673 page 61-62</p>	6,9